# ATTACHMENT B

Additions and corrections to given Papers I-V

## For Papers I-V:

[1.] The correct form for the y-axis of the standard Mollier (i,x) diagram as Salin-Soininen perspective transformation is shown in Paper V.

## For Papers II-IV:

[2.] The drying air heaters utilize the heat of both superheating and evaporation (of superheated extraction steam from steam turbine), and the heat of evaporation (of saturated backpressure steam from steam turbine). The condensate water from air heaters corresponds to the properties of saturated water at the corresponding pressure of steam [bar(a)].

[3.] The diameter of the wood sphere used in calculations is 10 mm, unless otherwise mentioned.

## For paper II:

[4.] Table 1: Heat capacity for peat dry solids is 1.6 kJ/ kg K  (Constant).

## For paper III:

[5.] P. 69:  In Equation (3), thermic efficiency should read thermal efficiency.

[6.] P. 75: Temperatures of condensated water from selected drying systems vary between 31.7 and 36.3 $^o$C  as outdoor temperature varies between $-15$ $^o$C and $+15$ $^o$C.

[7]. The thermodynamic properties of saturated air has been interpolated from values shown in Ref. (Keey, R.B., Drying Principles and Practice, 1972).

## For paper IV:

[8.] In all calculated results, the exhaust drying air temperature differences at the hot air saturation temperature in drying stages of  MSDSs ($t_{gout}$-$t_s$)$_i$ are 12 $^o$C.